

# ThermoFAST

Thermodynamic Calculation Tool

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## User Manual

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**Copyright:** Corey J. Baker; Eric F. May  
Fluid Science & Resources Division  
The University of Western Australia  
35 Stirling Hwy, Crawley, WA, 6009  
Website: <http://fsr.ecm.uwa.edu.au/>  
Email: [Eric.May@uwa.edu.au](mailto:Eric.May@uwa.edu.au)

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## 1 Introduction

ThermoFAST is a thermodynamic property calculator for LNG and natural gas with the ability to perform vapour-liquid-solid equilibrium calculations, predict conditions at which solid formation can occur in complex, multi-component systems and generate full phase envelopes.

If more information regarding the thermodynamic models or algorithms used in ThermoFAST, please refer to the following Doctoral Thesis.

Baker, CJ 2018, *Phase equilibrium measurements and advanced modelling for optimising liquefied natural gas production*, Doctor of Philosophy, The University of Western Australia. <https://doi.org/10.26182/5bc411e7ccc0d>

## 2 Developers

Name	Role	Email
<b>Corey Baker</b>	Lead Software Developer The University of Western Australia	<a href="mailto:Corey.Baker@research.uwa.edu.au">Corey.Baker@research.uwa.edu.au</a>
<b>Eric F. May*</b>	Chevron Chair of Gas Processing The University of Western Australia	<a href="mailto:Eric.May@uwa.edu.au">Eric.May@uwa.edu.au</a>

\* Corresponding author

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**Australian Government**  
**Australian Research Council**

## 4 Installation Folders

All the following files and folders must be stored in the same directory in order to utilise them internally; however only the “**ESSENTIAL**” components are required to run ThermoFAST.

Name	Type	Description
<b>ThermoFAST.exe</b>	<b>ESSENTIAL</b>	Primary executable
<b>TREND.dll</b>	<b>NOT ESSENTIAL</b>	Provides access to the reference equation of state GERG-2008 and improved Combustion Gas equations powered by TREND*
<b>ThermoFAST</b> [Folder]	<b>NOT ESSENTIAL</b>	Folder that provides ThermoFAST with quick access to the following sub-folders <ol style="list-style-type: none"> <li>1. Saved Files</li> <li>2. Custom Binary Interaction Parameters</li> <li>3. Custom Component Properties</li> <li>4. Custom Fluid Files</li> <li>5. Documents</li> </ol>

\* Span, R.; Eckermann, T.; Herrig, S.; Hielscher, S.; Jäger, A.; Thol, M. (2016): TREND. Thermodynamic Reference and Engineering Data 3.0. Lehrstuhl für Thermodynamik, Ruhr-Universität Bochum.

## 5 Menu Items

### 5.1 File

Name	Description
<b>Save</b>	Saves the current configuration using the previous save or load file name and location including units, component properties, models, composition, flash and solid calculations including solid diagrams. It is recommended to save to the recommended file location for quick and efficient access. If no previous saves or loads have been performed on the current instance of ThermoFAST then the <i>Save As</i> function will be utilised.
<b>Save As</b>	Save a new case folder to the recommended or a custom directory
<b>Load</b>	Loads a previously saved case folder. The <i>Load</i> function loads a saved folder of .txt files and therefore it is necessary to open the desired <i>Load</i> folder and then simply click open again once the .txt files appear. This will

<b>Name</b>	<b>Description</b>
	load all the required files in the selected case folder. It is not necessary to select any of the individual .txt files.
<b>Reset</b>	Resets the window to the default settings (deleting all selected components and calculation results)
<b>Exit</b>	Exits ThermoFAST, closing all associated windows



TIP # 1: Saving to the recommended file location will cause previous cases to appear in the drop down menu located in the “Load” function for quick access

## 5.2 Models

<b>Name</b>	<b>Description</b>
<b>Equation of State</b>	Selected equation of state, where the recommended package tuned for solid predictions is Peng-Robinson (1976).
<b>Mixing Rules + Interaction Parameters</b>	Selected type of mixing rule in the drop-down box. The button ‘View’ button loads multiple data sets containing binary interaction parameters (BIPs) available for user selection. In some versions of ThermoFAST the user is able to edit the BIPs and save a data set for future quick access.
<b>Solid Equilibrium</b>	Type of approach taken for solid equilibrium calculations. The default approach utilises the cubic equation of state to calculate the fugacity of the solvent. Other methods (not available in ThermoFAST) use activity coefficient models.
<b>Solid Density</b>	Selected model for density of a pure solid
<b>Hydrates</b>	Selected hydrate model. Only available in specific versions of ThermoFAST; please contact the developers or visit their website for information on how to obtain this version. TREND has an inbuilt hydrate model that utilises the Helmholtz equation in the Improved Combustion Gas version only



TIP # 2: If a custom binary interaction parameter data set is saved by the user it will appear in the **ThermoFAST/Custom Binary Interaction Parameters** folder in the same directory as ThermoFAST.exe

## 5.3 Help

Name	Description
<b>User Manual</b>	Obtain a copy of this user-manual through the user interface
<b>About Us</b>	Description of ThermoFAST and acknowledgements
<b>Contact Developers</b>	Contact the developers for future updates and troubleshooting
<b>How to Cite us</b>	Shows the citation for the current version of ThermoFAST
<b>Disclaimer</b>	ThermoFAST's official disclaimer regarding the appropriate use of this product



TIP # 3: A copy of the user manual will be saved in the **ThermoFAST/Documents** folder in the same directory as ThermoFAST.exe

## 6 User Interface

### 6.1 Units

Name	Description
<b>SI (K, MPa, mol, J)</b>	Custom set of International System inspired units tailored to academic and research areas (metric)
<b>SI (°C, bar, kg, J)</b>	Custom set of International System inspired units tailored to plant and operational data (metric)
<b>Field (°F, psia, lbmol, BTU)</b>	Custom set of Field (Imperial) units
<b>Custom</b>	Allows the user to select a combination of units based on preference; composition, temperature, pressure, density, heat capacity and enthalpy. Heat capacity and Heat of Fusion (units of enthalpy) are required in the calculation of solid equilibrium.

### 6.2 FLUID

Name	Description
<b>Fluid</b>	Choose a saved fluid (if applicable), otherwise a custom mixture is automatically created
<b>Available</b>	Global list of available components
<b>Selected</b>	Components that have been selected for calculations
<b>&lt; Move Selected &gt;</b>	Selected components will be moved to the opposite list

<b>Name</b>	<b>Description</b>
<b>CLEAR ALL</b>	Remove all “Selected” components. Note this will reset various outputs associated with this mixture.
<b>EDIT COMPONENT PROPRERTIES</b>	View or edit the selected component properties depending on the version of ThermoFAST. Save functionality is available in the editable version allowing users to save custom sets to the “Custom Component Properties” folder. If a name already exists it will overwrite that data set.
<b>Allow Ice to Form</b>	This checkbox appears when a mixture containing water is selected. The formation of ice from trace concentrations of water in LNG mixtures at cryogenic temperatures is difficult to measure and not well understood. Standard industry specifications for the maximum allowable water content in LNG to avoid ice formation are in the range 0.1 to 1 ppm. However, at these trace concentrations most thermodynamic models capable of predicting solid ice formation indicate ice should be stable at temperatures as high as 200 K. If the user is interested in the formation of other cryogenic solids then it is advisable to leave this box unchecked. This option only applies to the 'FLASH' and 'SOLIDS' calculators.



TIP # 4: Multiple components can be selected by holding down control and/or shift



TIP # 5: Double clicking a component moves it to the opposite list



TIP # 6: If a component property data set is saved by the user it will appear in the

**ThermoFAST/Custom Component Properties** folder in the same directory as ThermoFAST.exe


## 6.3 COMPOSITION

<b>Name</b>	<b>Description</b>
<b>Fluid</b>	Choose a saved fluid (if applicable), otherwise a custom mixture is automatically created


<b>Name</b>	<b>Description</b>
<b>Basis</b>	Select the composition basis: mass or molar
<b>Save Fluid</b>	Saves a custom defined fluid and a range of compositions. The fluid is saved in a location that allows ThermoFAST quick access.
<b>Delete Saved Fluid</b>	Deletes the fluid that is currently selected. If the “custom mixture” is selected it will simply wipe all data.
<b>Allow Ice and Hydrates to Form</b>	This checkbox appears when a mixture containing water is selected. The formation of ice from trace concentrations of water in LNG mixtures at cryogenic temperatures is difficult to measure and not well understood. Standard industry specifications for the maximum allowable water content in LNG to avoid ice formation are in the range 0.1 to 1 ppm. However, at these trace concentrations most thermodynamic models capable of predicting solid ice formation indicate ice should be stable at temperatures as high as 200 K. If the user is interested in the formation of other cryogenic solids then it is advisable to leave this box unchecked. This option only applies to the 'FLASH' and 'SOLIDS' calculators.
<b>VIEW PHASE ENVELOPE</b>	Calculates the phase envelope of the mixture in the adjacent option box in the case of multiple compositions.
<b>NORMALISE</b>	Normalise all compositions - this is not essential but can be helpful
<b>CLEAR ALL</b>	Clears all compositions but does not clear selected components
<b>COPY DATA</b>	Copy all compositions and component names to the clipboard for easy integration into Excel
<b>Normalised Status</b>	Checks whether all compositions sum to 1 or zero

 TIP # 7: Multiple mixtures can be considered by simply entering in a new composition in each subsequent column.

 TIP # 8: Calculations will run with un-normalised compositions (they are normalised internally).


 TIP # 9: Users can select what data to copy to the clipboard by simply right clicking any selected data and pressing “copy” or using the shortcut “control” + “c”. Then simply right click in Excel and click “paste” to output the data, or use the shortcut “control” + “v”.




 TIP # 10: If a custom fluid and a range of compositions is saved by the user it will appear in the ThermoFAST/Custom Fluid Files folder, located in the same directory as ThermoFAST.exe

## 6.4 FLASH

Name	Description
<b>CONDITIONS</b>	Performs flash calculations at a specified temperature and pressure to output the phase fractions and properties
<b>COMPONENTS</b>	Outputs the compositions of the component phases
<b>Component Amounts</b>	Select the component unit basis: mass or molar basis
<b>Mixture Number</b>	Corresponds to the mixture number under the “COMPOSITION” tab
<b>LOCATE</b>	<p><b>Temperature-Pressure Flash:</b> perform a T-P flash</p> <p><b>Bubble Point Temperature:</b> locates the bubble point temperature at a given pressure and composition</p> <p><b>Bubble Point Pressure:</b> locates the bubble point pressure at a given temperature and composition</p> <p><b>Dew Point Temperature:</b> locates the dew point temperature at a given pressure and composition</p> <p><b>Dew Point Pressure:</b> locates the dew point pressure at a given temperature and composition</p>
<b>Locate _____</b> <b>(Checkbox that appears)</b>	Appears when a bubble or dew point calculation is selected. In some systems there may be two conditions at which a dew or bubble point exists at the specified temperature or pressure. Selecting this checkbox will force the algorithm to return the condition that satisfies the nominated constraint; if it is unchecked, the returned condition will be the other possibility if one exists.
<b>CALCULATE</b>	Performs the desired calculation
<b>CLEAR ALL</b>	Deletes all inputs and outputs
<b>COPY DATA</b>	Copy all inputs and outputs to the clipboard for easy integration into Excel

 TIP # 11: Although the mixture number is unique to each composition, if more flash conditions exist than there are mixture numbers, it will simply perform a flash calculation on the composition associated with the most recent mixture number. Therefore, there is no need to re-enter the same composition to perform multiple flash calculations of the same mixture.

 TIP # 12: If more than one solid component exists then a combined solid density will be shown; however this is only used as an indicator. Unlike vapour and liquid phases, solids are not homogenous mixtures and each solid compound is treated as a separate solid phase (for this reason the “COMPONENTS” tab reports solid fractions, rather than the solid composition). The density of the individual solid can be found by simply choosing the pure component and specifying the same temperature and pressure.

## 6.5 SOLIDS

ThermoFAST is able to locate solid transition region temperatures or maximum solid concentrations for the selected mixture number. It has the ability to locate different types of solid phase equilibrium; solid-vapour, solid-vapour-liquid and solid-liquid equilibrium (solid-solid can be found under a normal “FLASH” calculation). The algorithm searches at constant pressure for the highest temperature at which a solid phase appears; thereafter it searches for and reports subsequent phase transitions that occur at lower temperatures. A detailed description of all possible transitions that can be located is provided in section 6.5.3 with illustrations.

### 6.5.1 SEARCH


Name	Description
<b>TEMPERATURE</b>	<p>Used to specify and report the search results for the temperatures at which solid phase transitions occur for a given mixture at a specified temperature. The user must specify the pressure at which to search (“Input Pressure”).</p> <p>Multiple pressures or multiple mixture numbers can be specified.</p> <p><b>Locate Melting Temperature at Bubble Point Pressure:</b></p> <p>If checked, ThermoFAST will search for the triple point condition where the bubble point meets the melting point. Solid equilibrium experiments are often conducted along the liquid’s bubble point curve and in many</p>

Name	Description
<b>CONCENTRATION</b>	<p>cases the system pressure is not reported. For this search the composition of the liquid phase (rather than the overall composition) must be specified. Computation can be slow and this triple point may not exist in all systems which will result in an unstable condition.</p> <p>Used to specify and report the search results for the maximum mole fraction of the solute that the solution can hold at the specified temperature and pressure. The user must specify the temperature and pressure (“Input Temperature” and “Input Pressure”) at which to calculate the solute concentration. The user can also specify a different solute to that recommended using the drop down menu. Multiple pressures or multiple mixture numbers can be specified. In cases where the algorithm is becomes unstable a range of melting temperatures or concentrations at the specified pressure. The user also has the option of additionally viewing all temperatures at which a phase transition occurs at the given pressure and calculated composition.</p>
<b>CALCULATE</b>	Executes the search algorithm selected via either “ <b>TEMPERATURE</b> ” or “ <b>CONCENTRATION</b> ” above.
<b>CLEAR ALL</b>	Deletes all search inputs and outputs for the solids search
<b>COPY DATA</b>	Copy all solid search inputs and outputs to the clipboard in a format easily pasted into Excel.
<b>DICTIONARY OF PHASE TRANSITIONS</b>	Provides descriptions of the phase transitions that may be returned by the solids search algorithm, similar to those provided in section 6.5.3

### 6.5.2 GRAPH

Name	Description
<b>GRAPH</b>	Allows the user to calculate solubility curves, solid phase diagrams and a eutectic diagram (temperature-composition plot) for a selected mixture

<b>Name</b>	<b>Description</b>
<b>Selected Mixture</b>	Performs the calculations with the mixture number corresponding to the “COMPOSITION” tab
<b>SOLUBILITY</b>	Calculates a solubility curve for the selected mixture at a constant pressure. The user is able to choose the solute that will solidify. Solidification of other components in the mixture will then not be considered by the calculation. The user selects concentration unit type and a range of concentration over which to calculate the corresponding melting temperature. For binary systems it is not necessary to specify the mixture composition because the solvent is sufficiently defined.
<b>SOLID PHASE</b>	Calculates a pressure-temperature diagram for a given mixture at which the solid phase transitions are indicated. The mixture composition must be defined. Essentially the Solid Search function is executed at the number of pressures specified by the user within the selected pressure range.
<b>EUTECTIC</b>	Calculates a graph containing the different solid transition regions versus the selected component’s composition. This will also locate the eutectic point where composition of the selected component produces the mixture’s lowest melting temperature (Eutectic Temperature). This search also locates triple points.
<b>CALCULATE</b> _____	Calculates the selected graph if sufficient information is has been provided by the user.
<b>SHOW GRAPH</b>	This button will appear upon completion of the graphing calculation, allowing the user to view the results.

 **TIP # 13:** The user is able to copy the graph’s outputs to the clipboard for easy integration to Excel once the “SHOW GRAPH” button is pushed

### 6.5.3 TYPES OF TRANSITION POINTS

Table 6.1 presents the Baker-May classification of transition pathways related to solid-fluid equilibrium that were identified using ThermoFAST. The classification also indicates whether

each transition pathway can be the highest solid-fluid equilibrium temperature (HSET) and/or occur at a temperature below the HSET. Some of these transition pathways are only possible in multi-component mixtures as a consequence of Gibbs Phase rule. Correctly identifying which type of transition is associated with the appearance of a solid phase at a given condition is important in an LNG production context because processing in upstream operations can in principle produce a fluid mixture containing no solids that is initially at a condition below its HSET. Please refer to the following Doctoral Thesis for further detail on the Baker-May classification table:

Baker, CJ 2018, *Phase equilibrium measurements and advanced modelling for optimising liquefied natural gas production*, Doctor of Philosophy, The University of Western Australia.  
<https://doi.org/10.26182/5bc411e7ccc0d>

Table 6.1: The Baker-May classification of transition pathways involving solid-fluid equilibrium for pure fluids and mixtures. The ability for the transition to be the highest solid-fluid equilibrium temperature (HSET) and/or occur at a temperature below HSET is also indicated.

<i>Path</i>	<i>Can be HSET?</i>	<i>Can be below HSET?</i>	<i>Description of Transition</i>
<b>Pure Fluids Only<sup>#</sup></b>			
#1	True	False	Liquid to Solid*
#2	True	False	Vapour to Solid*
<b>Multicomponent Mixtures (<math>\geq 2</math> components)</b>			
#3	True	False	Vapour to SVE
#4	True	False	VLE to SVE
#5	True	True	Liquid to SLE
#6	True	False	Liquid to SLE (Liquid Retrograde)
#7	False	True	SLE (Liquid Retrograde) to SVE (SLVE)
#8	False	True	SVE to SLE (SLVE)
#9	False	True	SVE to SLE (Solid Retrograde)
#10	False	True	SLE (Solid Retrograde) to SLE (Normal)^
#11	False	True	SVE to SVE (Solid Retrograde)^
#12	False	True	SVE to VLE (SLVE) [or SVE (Solid Retrograde) to VLE]
#13	False	True	VLE to Liquid
#14	False	True	SLE (Solid Retrograde) to Liquid
#15	False	True	SVE to Liquid [or SVE (Solid Retrograde) to Liquid]
<b>Multicomponent Mixtures (<math>\geq 3</math> components)</b>			
#16	True	False	VLE to SLVE (Liquid Retrograde)
#17	True	False	VLE to SLVE
#18	False	True	SLE (Liquid Retrograde) to SLVE
#19	False	True	SLE (Liquid Retrograde) to SLVE (Liquid Retrograde)
#20	False	True	SLVE (Liquid Retrograde) to SVE
#21	False	True	SLVE to SLE (Solid Retrograde)
#22	False	True	SLVE to SLE
#23	False	True	SVE to SLVE
#24	False	True	SVE to SLVE (Solid Retrograde)
#25	False	True	SLVE (Solid Retrograde) to Liquid
#26	False	True	SLVE (Solid Retrograde) to VLE

<sup>#</sup> Binary mixtures at their Eutectic compositions can also undergo these transitions

\* the special case of a pathway that passes through the pure fluid's triple point is considered an intersecting subset of pathway #1 and #2

^ Pathways are not phase transitions since no new phase appears. They are termed "retrograde-only transitions" as they correspond to the location of either a minimum or a maximum in the amount of solid phase with decreasing temperature

## 6.6 TUNE


The user has a powerful tool for tuning the binary interaction parameters for specific component sets using the selected equation of state. The user can tune to solid formation and bubble point conditions, as well as vapour-liquid compositions. The user will then be able to manually add these tuned binary interaction parameters to custom data sets under the *Models* menu item.

Name	Description
<b>BINARIES</b>	Select the components to tune and set the starting binary interaction parameters based on the selected mixing rule. A good initial estimate may be required, this is common practice when using a multi-parameter mixing rules. It is recommended to use a higher starting value for solid data ( $0.01 < k_{ij} < 0.1$ and $C_{ij} = 1$ ).
<b>CRITERIA</b>	Select from a variety of data types to tune from including solid formation, bubble point conditions and vapour-liquid compositions. Select the type of objective function (absolute or relative), absolute is recommended for vapour-liquid composition data. Select the tolerance of the binary interaction parameter(s) and the maximum number of iterations before stopping the calculation.
<b>DATA</b>	Input the data that ThermoFAST will use to tune the binary interaction parameter(s). The sub-categories represent the objective functions selected under <i>CRITERIA</i> . In regards to <i>SOLID</i> data, the user may also tune to the triple point for solid calculations (the boundary at which the bubble point meets the melting point and therefore a pressure is not required).
<b>CLEAR ALL</b>	Deletes all inputs and outputs (resets the tuning interface)
<b>COPY DATA</b>	Copy the tables under <i>DATA</i> or <i>OUTPUTS</i> to the clipboard for easy integration into Excel

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<b>Name</b>	<b>Description</b>
<b>OUTPUTS</b>	View the tuning results. The user can view the optimised binary interaction parameter and results as the tuning is progressing (before the completion criteria is met).

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 **TIP # 14:** If the tuning calculation has ended, the user can simply click TUNE DATA again to begin tuning to the most recently optimised binary interaction parameter and these are updated under the BINARIES tab.